Pretreatment Technologies

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Outline

- 1. Cellulosic Biofuels 30,000 ft view
- 2. Pretreatment : Keystone of Biological Route
- 3. Pretreatment Technologies: Overview
- 4. Process Considerations
- 5. Conclusions
- 6. Questions



Biofuel Production Strategies

Biochemical Conversion

- Conversion by living system
- Fermentation
- Biogas, Ethanol, etc
- Thermochemical Conversion
 - Conversion by catalysts and/or heat
 - Pyrolysis, direct combustion, gasification



BIOLOGICAL CONVERSION

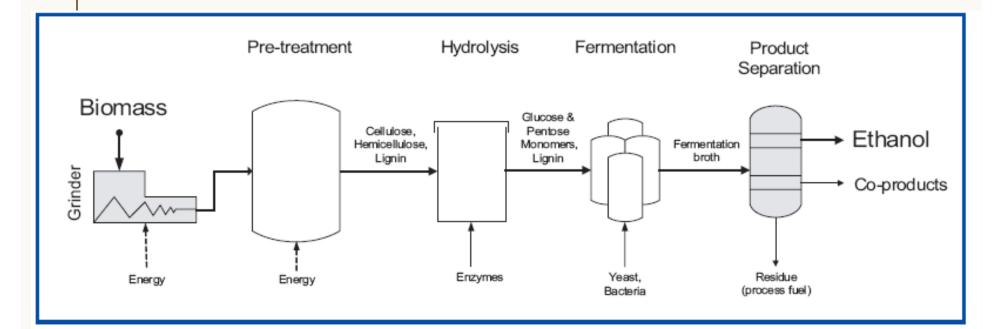


Figure from US DOE



Biological Route from Biomass to Biofuels

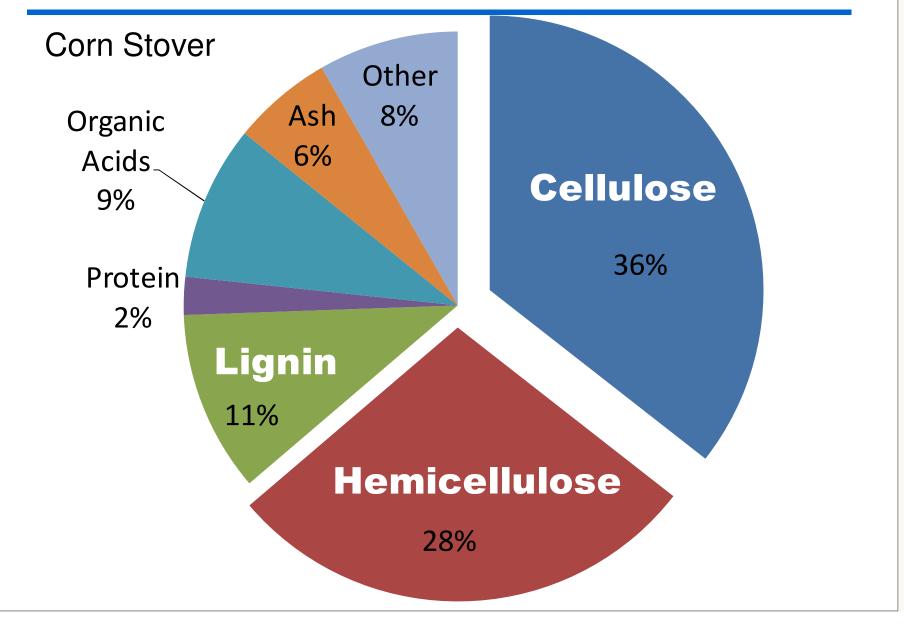
 Use natural or modified biocatalysts to convert carbohydrates to <u>fuel</u>

 Break long polymers of sugars (cellulose and hemicellulose) into individual sugars

Ferment sugars to biofuel molecules



Lignocellulosic Biomass



Plant Cell Wall Polysaccharides

- Source of fermentable sugars
 - Hexoses (glucose)
 - Pentoses (xylose)
- Recalcitrant to hydrolysis by <u>consortium of enzymes</u>
- Materials handling (viscosity)
- Source of inhibitors of enzymes and fermentation
 - Present in biomass (phenolic acids, acetate)
 - Derived from biomass during processing (furfural, HMF)



Biological Route: Fuels

> Ethanol

- Various microbes (yeast and bacteria)
- Current king of biofuels (corn, cane, beet)

Butanol

- Clostridia sp. bacteria
- Mixed solvent fermentation (butanol, acetone, ethanol)

Others

- Organic acids upgraded via thermochemistry (Mixalco)
- Amyris Biotechnologies
- LS9, GEVO, etc.



Pretreatment: Keystone of the Biological Route

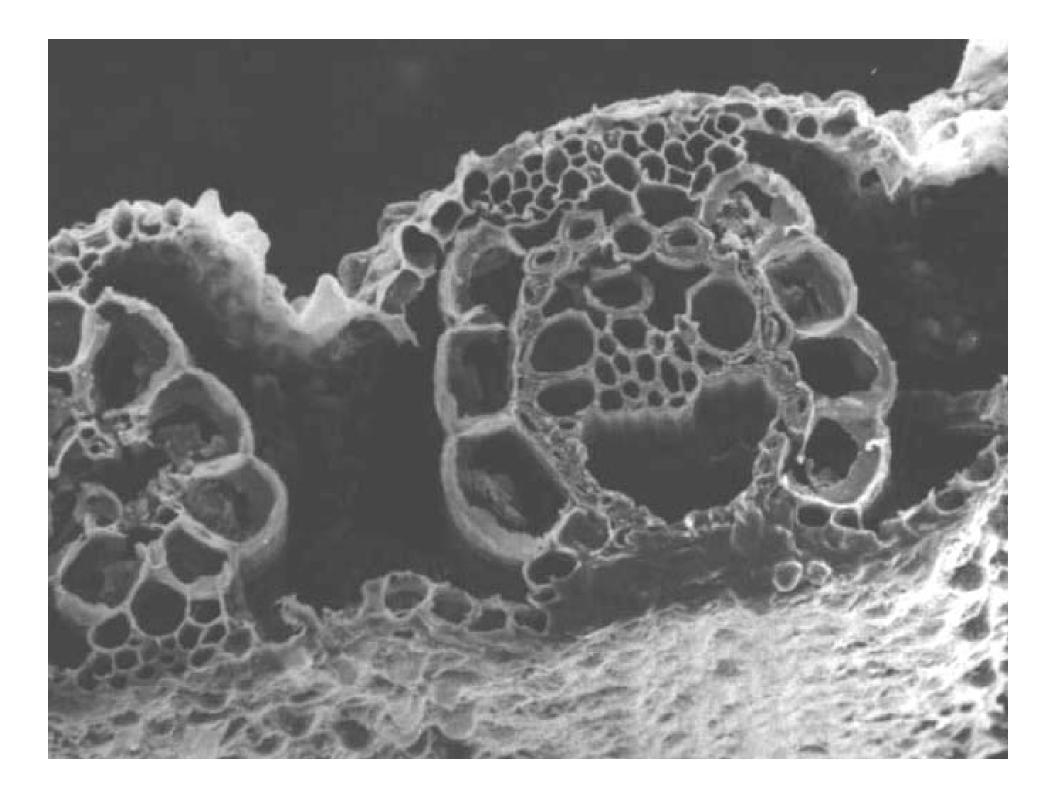
- Overcoming recalcitrance of biomass to hydrolysis (saccharification)
- > Multiple technologies, varying mechanisms
- Increase <u>rate</u> of hydrolysis (release of sugars)
- Increase <u>yield</u> of sugars
- Commodity chemical yield, yield, yield!

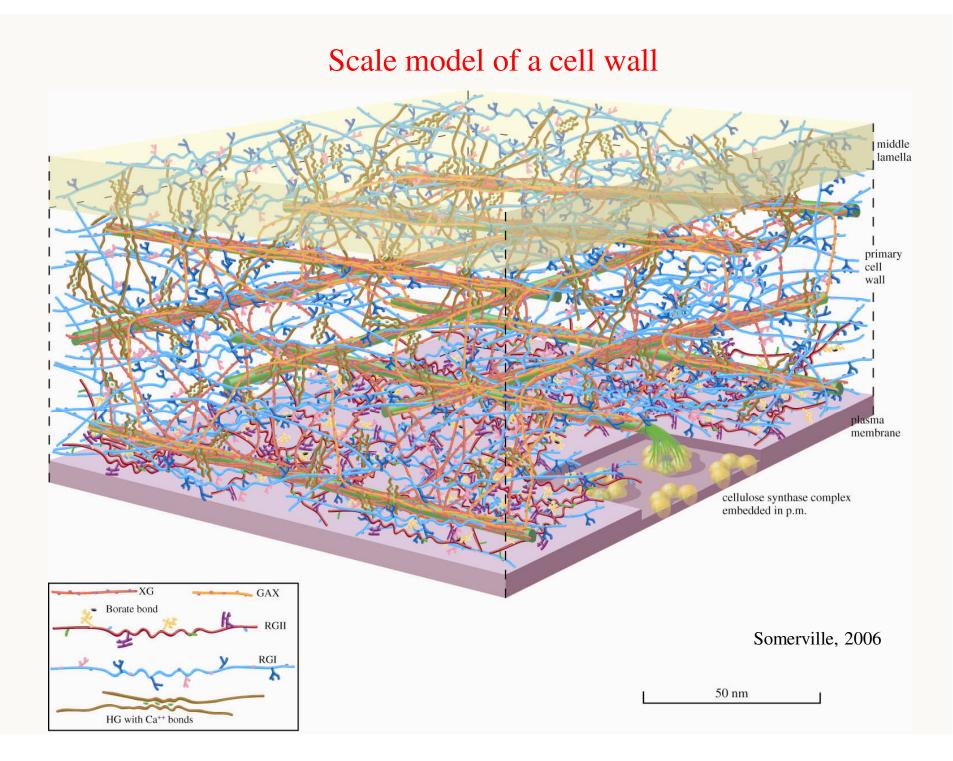


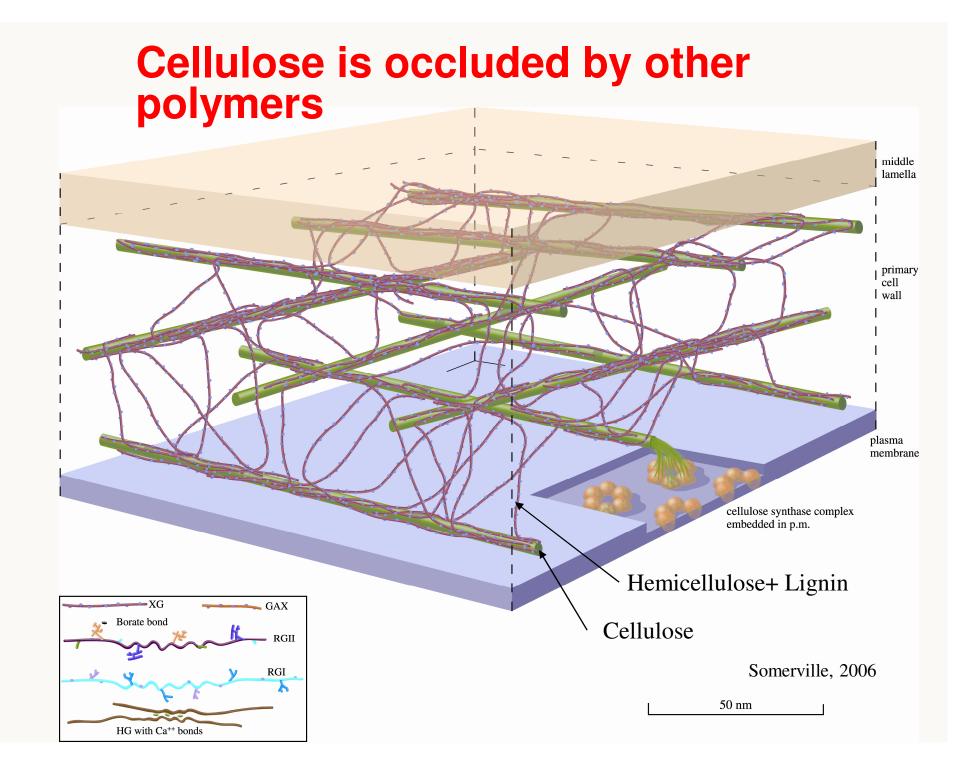
Pretreatment Keystone of Biological Route

- Affects chemical makeup of feedstock
- Affects physiochemical interactions between feedstock constituents
- > Affects fermentation performance
 - Inhibitors generated by pretreatment (furfural, HMF)
 - Inhibitors inherent to feedstock (acetate, phenolics, etc.)

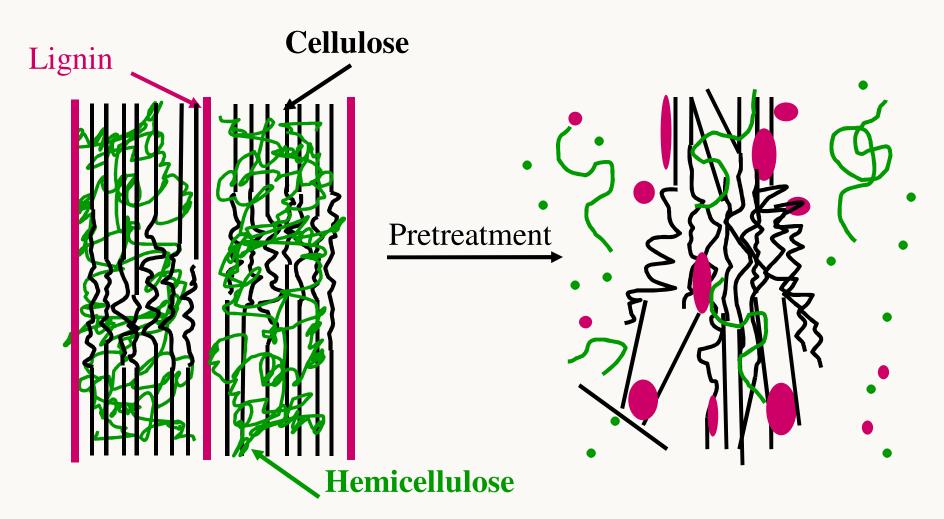








Simplified Impact of Pretreatment on Biomass



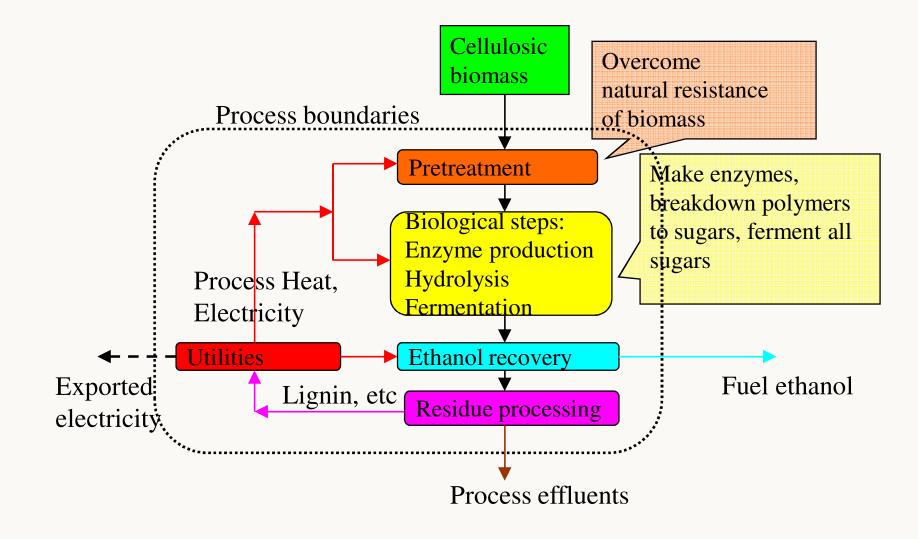
Mosier, N.; Wyman, C.; Dale, B.; Elander, R.; Lee, Y. Y.; Holtzapple, M.; and Ladisch, M. R. "Features of Promising Technologies for Pretreatment of Lignocellulosic Biomass," *Bioresource Technology* 96(6):673-686 (2005).

Overcoming Biomass Recalcitrance

- Remove or rearrange lignin
- Remove or rearrange hemicellulose
- Alter cellulose crystallinity / accessibility to enzymes improve reactivity
- Current technologies use a combination of chemicals and energy (thermal)



Enzymatic Conversion of Cellulosic Biomass to Ethanol



Factors Affecting Enzymatic Hydrolysis

Accessible beta bonds

- Higher accessibility of surface improves rate of attack by endo and exoglucanase
- > DP of pretreated cellulose
 - Lower DP favors higher ratio of exo to endo glucanase
- Lignin content
 - Blocks enzyme accessibility
 - Adsorbs enzyme non productively
- > End-product inhibition
 - Reduces rates and yields
 - Cellobiose and glucose particularly strong inhibitors

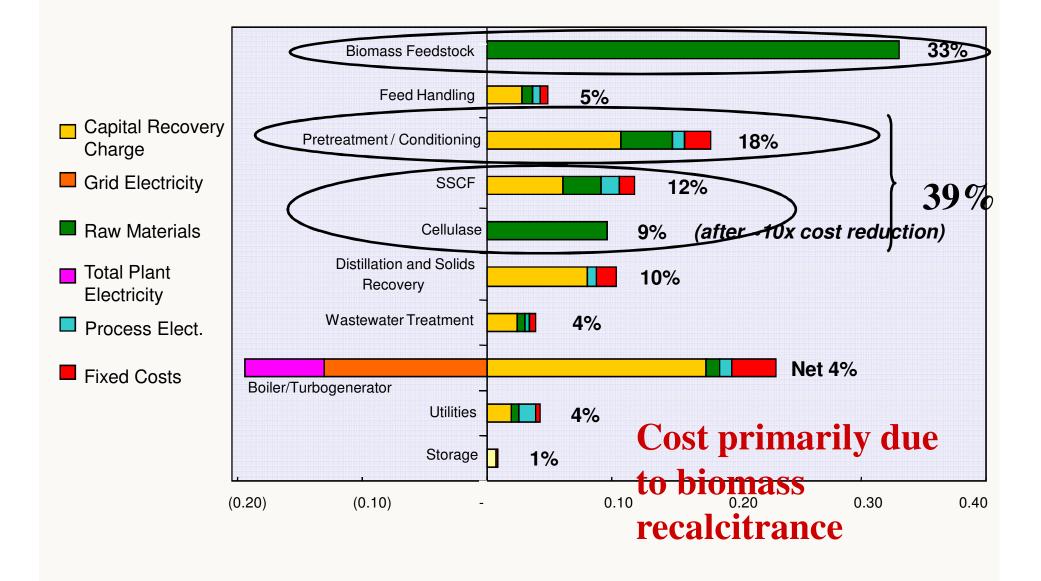


Pretreatment Goals

- Need to open up structure to make cellulose accessible to enzymes - high digestibility
- > High sugar yields from hemicellulose are also vital
- > Low capital cost pressure, materials of construction
- > Low energy cost
- Low degradation
- > Low cost and/or recoverable chemicals
- A large number of pretreatment technologies have been studied to improve cellulose digestion



Key Processing Cost Elements

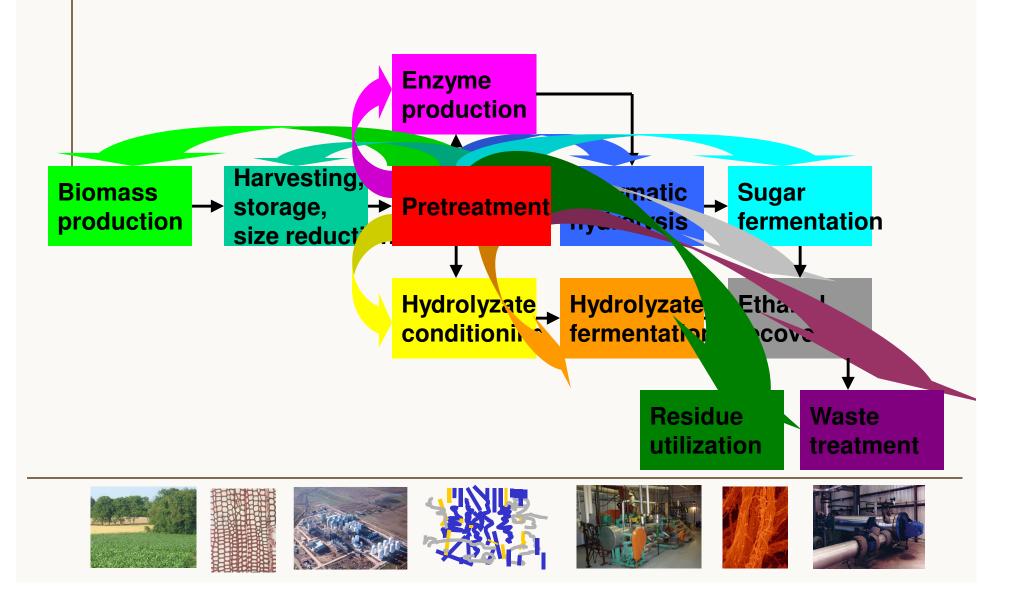


Importance of Pretreatment

- Although significant, feedstock costs are low relative to petroleum
- In addition, feedstock costs are a very low fraction of final costs compared to other commodity products
- Pretreatment is the most costly process step: the only process step more expensive than pretreatment is no pretreatment
 - Low yields without pretreatment drive up all other costs more than amount saved
 - Conversely enhancing yields via improved pretreatment would reduce all other unit costs

Need to reduce pretreatment costs to be competitive

Central Role and Pervasive Impact of Pretreatment for Biological Processing



Distinguishing Features of Pretreatment

- > Additives none, acid, base, solvent, enzymes
- > System physical, chemical, thermal, biological
- Operation batch/plug flow, continuous, flow through, countercurrent
- Solids concentration
- > Heat up method and time
- Cool down method and time
- Long on invention, short on fundamentals



Pretreatment Classes

Physical

Biological

Chemical



Physical Pretreatments

Size reduction

- Hammer mills
- Knife mills
- Extruders
- Disc refiners
- Planer
- Mechanical decrystallization
 - Ball mills
 - Roll mills
 - Dry mills
 - Colloid mills

Thermal

- Freeze/thaw
- Pyrolysis
- Cryomilling
- Radiation
 - Gamma rays
 - Microwaves
 - Electron beam
 - Lasers

Expensive and limited effectiveness





Biological Pretreatments

White Rot Red Rot Brown Rot

FomesfomentariusFomitopsisannosaPiptoparusbetulinus

PhellinusigniariusLaetiporussuphureus

GadodermaapplanatumTrametesquercina

ArmillariamelleaFomitopsispinicola

PleurotusostreatusGloephyllumsaepiarum

Attacks

lignin + + + cellulose + + -

Not very effective and require long times

Chemical Pretreatments 1

Oxidizing

- Peracetic acid
- Ozone
- Hydrogen peroxide
- Chlorine
- Sodium hypochlorite
- Chlorine dioxide

Concentrated acid

- Sulfuric (55-75%)
- Phosphoric (79-86%)
- Nitric (60-88%)
- Hydrochloric (37-42%)
- Perchloric (59-61%)

Cellulose solvents

- Inorganic salts
 - Lithium chloride
 - Stannic chloride
 - Calcium bromide
- Amine salts
 - Cadoxen

(cadmium chloride + ethylenediamine)

• Cooxen

(cobalt hydroxide + ethylenediamine)

Not cost effective

Chemical Pretreatments2

> Delignification

- Organosolv
 - Ethanol
 - Butanol
- Triethylene glycol
- Cellulose modification
 - Carboxymethyl cellulose
 - Viscose
 - Mercerized Many too expensive

Alkaline

- Sodium hydroxide
- Calcium hydroxide
- Kraft pulping
- Soda pulping
- Amines
- Ammonia
 - Gaseous
 - Liquid
 - Supercritical
 - •Aqueous
 - Percolation

Chemical Pretreatment 3

>Acids

Neutral pH

- Sulfite pulping
- Dilute sulfuric, phosphoric, or nitric acid
- Autohydrolysis with natural acids
- Liquid hot water
- Gaseous

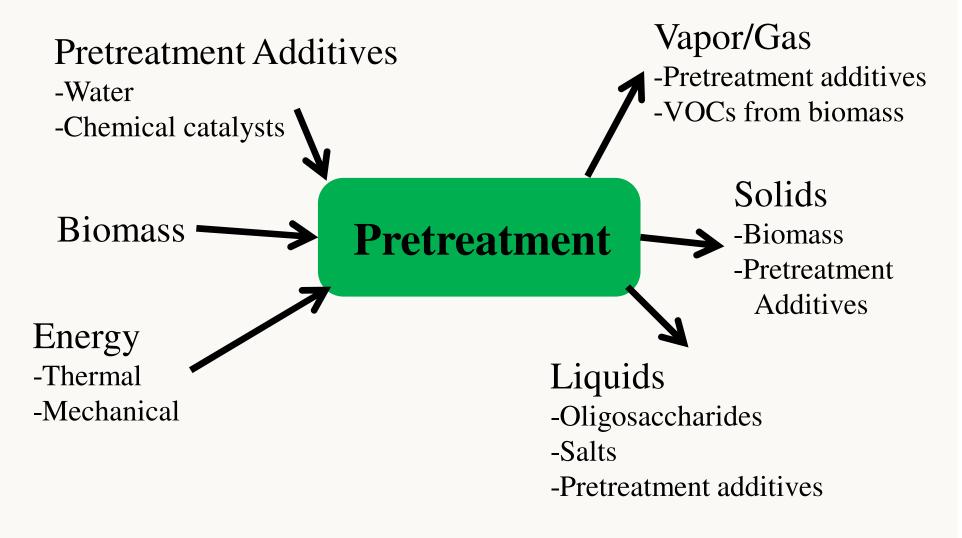
• *HCl, SO2, NO2, CO2*

Pretreatment with dilute acid currently favored

Challenges with Dilute Acid Pretreatment

- Cost of acid
- Cost to neutralize
- Need to remove toxics released and produced prior to biological steps
- > Expensive materials of construction
- Hemicellulose sugar yield limited to about 90%
- High enzyme dosages in subsequent cellulose digestion step
- Slow digestion of cellulose

Pretreatment Process



Pretreatment Additives

Solvents

- Water
- Acetone, Ethanol

Catalysts

- Acid
- Alkaline



Pretreatment Solvents

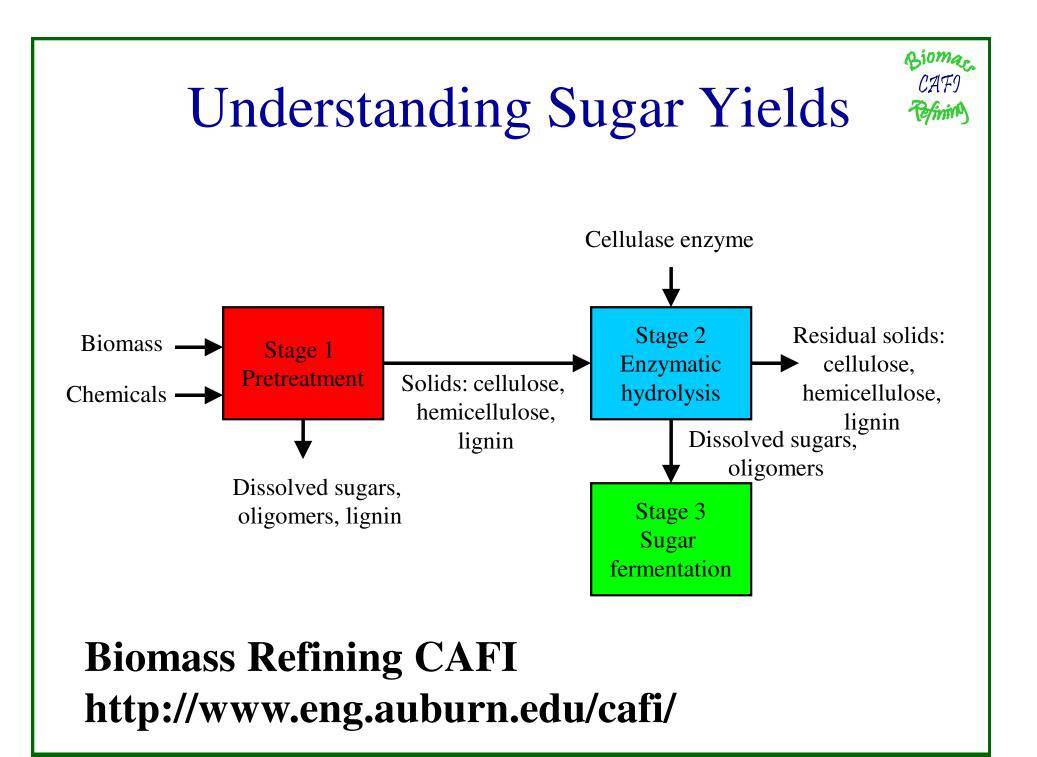
- Partial fractionation of biomass (solid into liquid)
- > Water
 - Most common solvent
 - Least expensive, compatible with downstream biological processing
- > Ethanol, acetone, others



Catalysts

- > Aid in hydrolyzing plant cell wall polymers
- > Lignin more susceptible to degradation via alkaline chemistry
- Hemicellulosemore susceptible to hydrolysis via acid chemistry
- Cost is key!
 - Acids: Sulfuric, phosphoric, hydrochloric
 - Bases: Sodium Hydroxide, Calcium Hydroxide, Ammonia







CAFI Pretreatments

- Acid
 - Dilute sulfuric acid in water (0.5 -1.0% w/w)
 - 140-220 C (285-428 F)
 - Pressurized to keep water in liquid phase
- Hot Water (Controlled pH)
 - 140-220 C (285-428 F)
 - Pressurized to keep water in liquid phase
 - Water acts as weak acid



CAFI Pretreatments

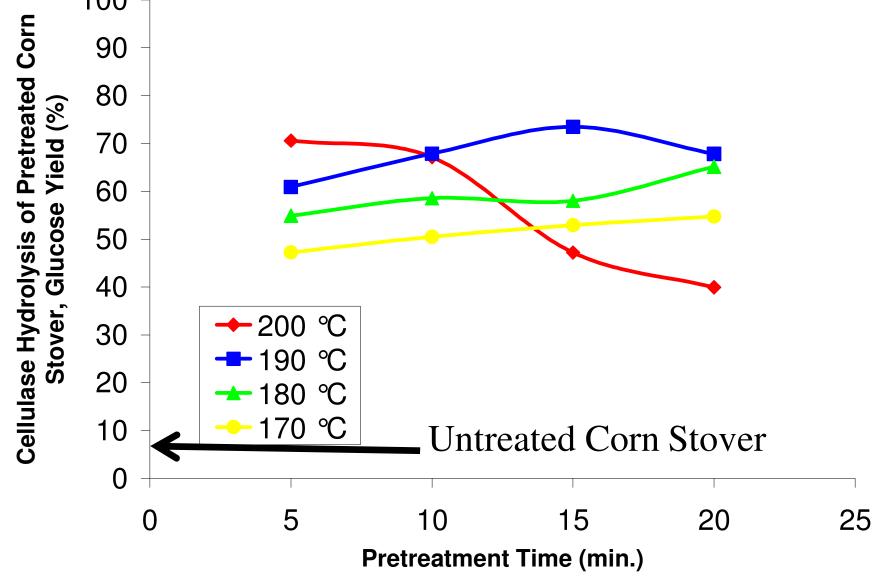
- Lime
 - Lime (calcium hydroxide) water slurry
 - Percolation bed
 - Temperatures 20-50 C (70-120 F)
- Ammonia Fiber Expansion (AFEX)
 - Dry-to-dry process
 - Liquid aqueous ammonia under pressure
 - -60-90 C (140-195 F)
 - Vaporize ammonia for recovery



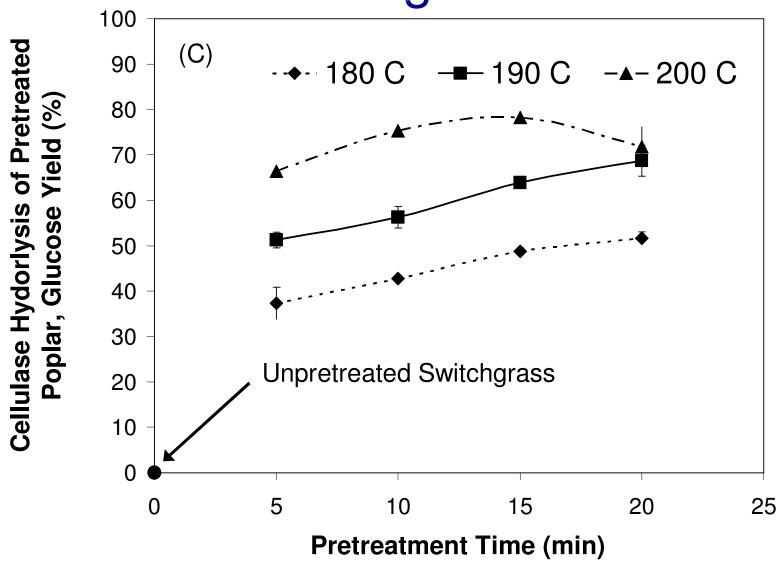
CAFI Pretreatments

- Sulfur Dioxide Steam Explosion
 - Sulfur dioxide 3%, soaked overnight
 - Temperature 190 C
 - 3 minutes reaction time
- Aqueous Ammonia Recycle Pretreatment
 - Ammonium hydroxide 15%
 - Temperature 180 C
 - Reaction time 27.5 minutes

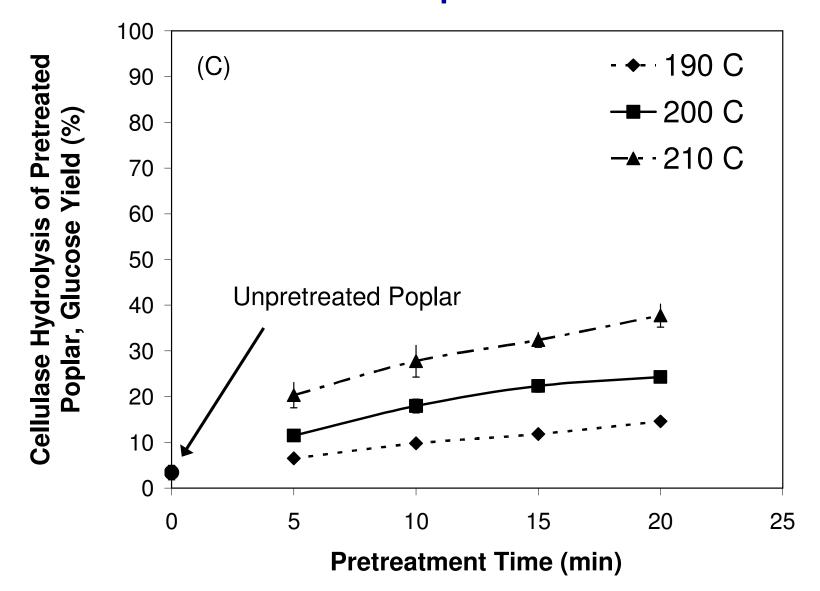
Glucose Yield of Liquid Hot Water (LHW) Pretreated Corn Stover



Glucose Yield of LHW Pretreated Switchgrass



Glucose Yield of LHW Pretreated Poplar



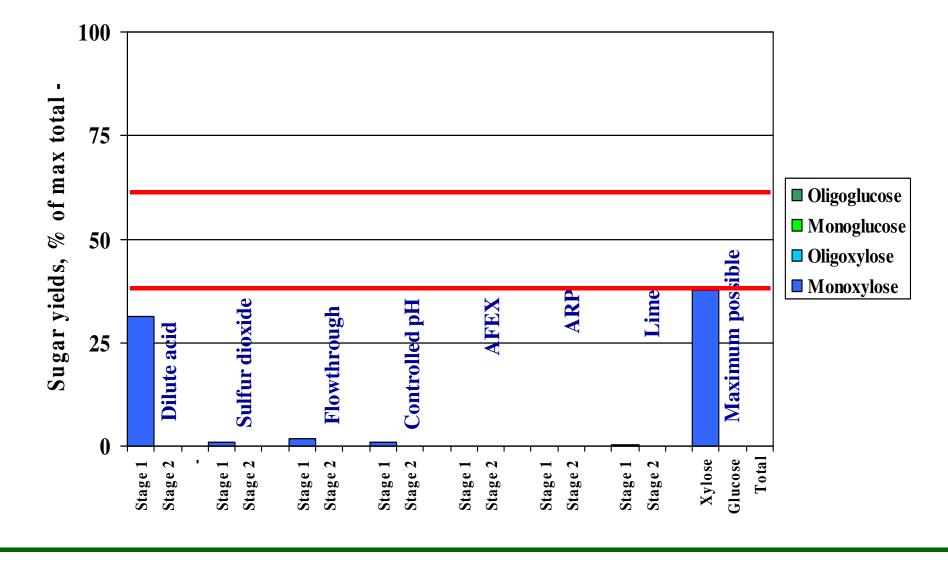
Enzymes Used and Experimental Conditions

Dioma

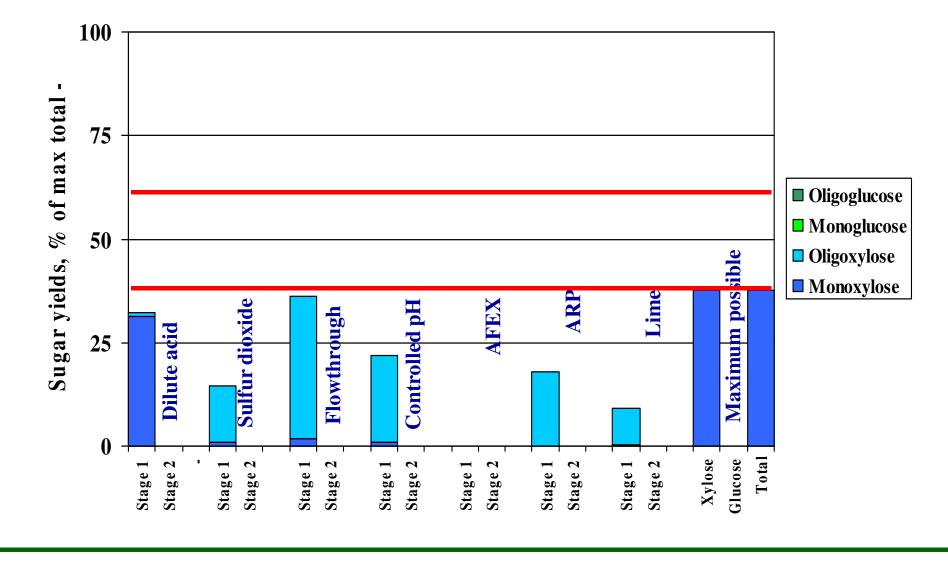
• Enzymes from Genencor International

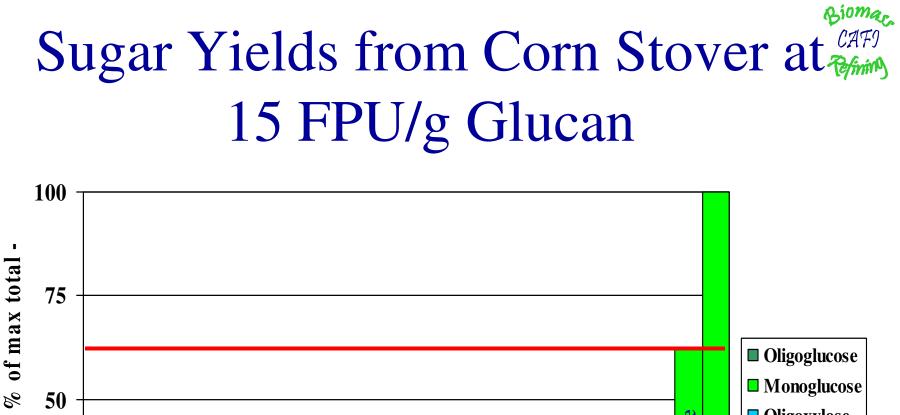
- o Spezyme CP (59 FPU/ml, 123 mg protein/ml)
- o GC-220 (89 FPU/ml, 184 mg protein/ml)
- o β -glucosidase (32 mg protein/ml)
- o Multifect Xylanase (41 mg protein/ml)
- Experimental conditions
 - o 1-2% glucan in 100 ml flasks in citrate buffer plus antibiotics
 - o Digestion time 72 hrs
 - o CBU : FPU ~ 2.0
 - o Enzyme loadings 3.0, 7.5,15, 50, and 60 FPU/g glucan prior to pretreatment

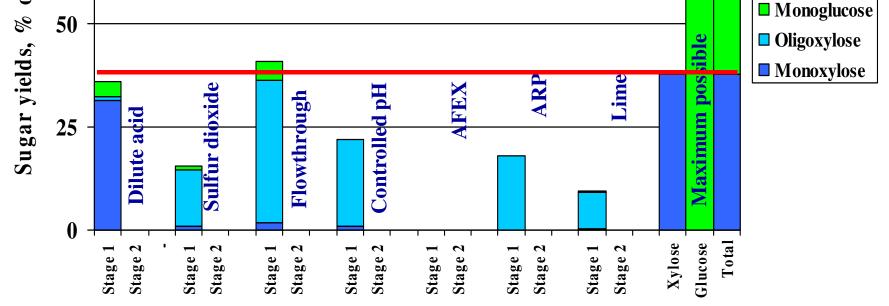
Sugar Yields from Corn Stover at CAF9 15 FPU/g Glucan

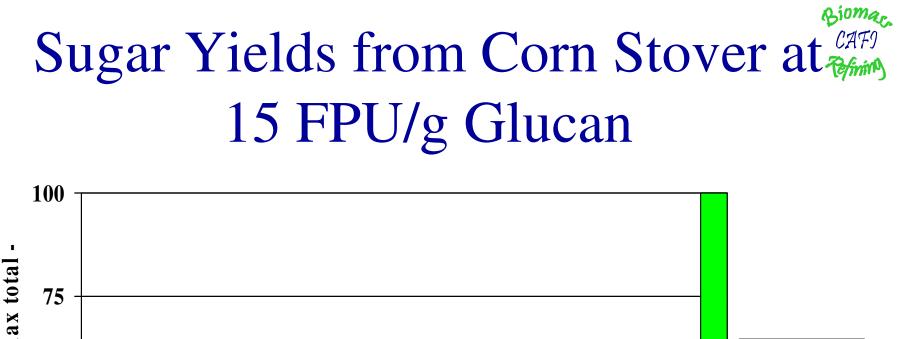


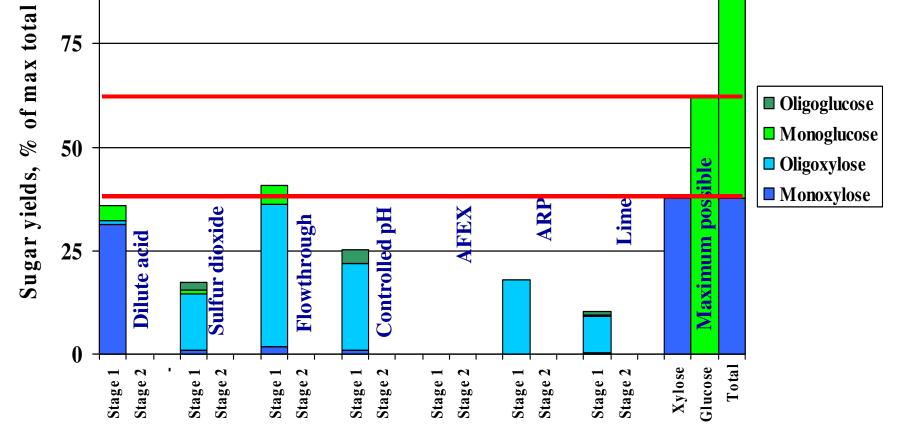
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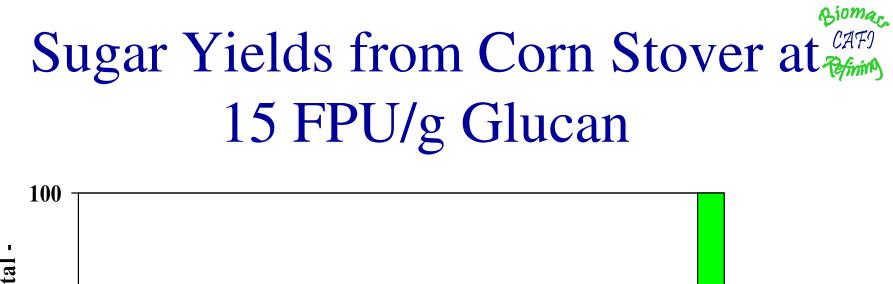


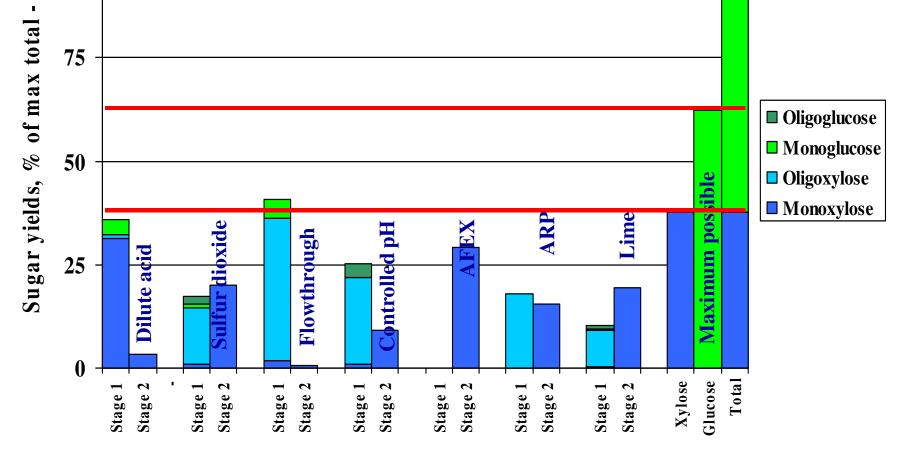




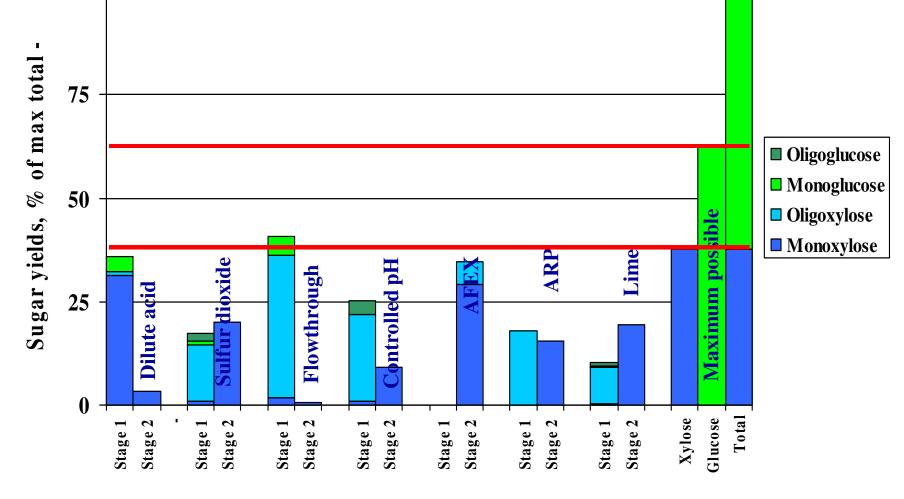


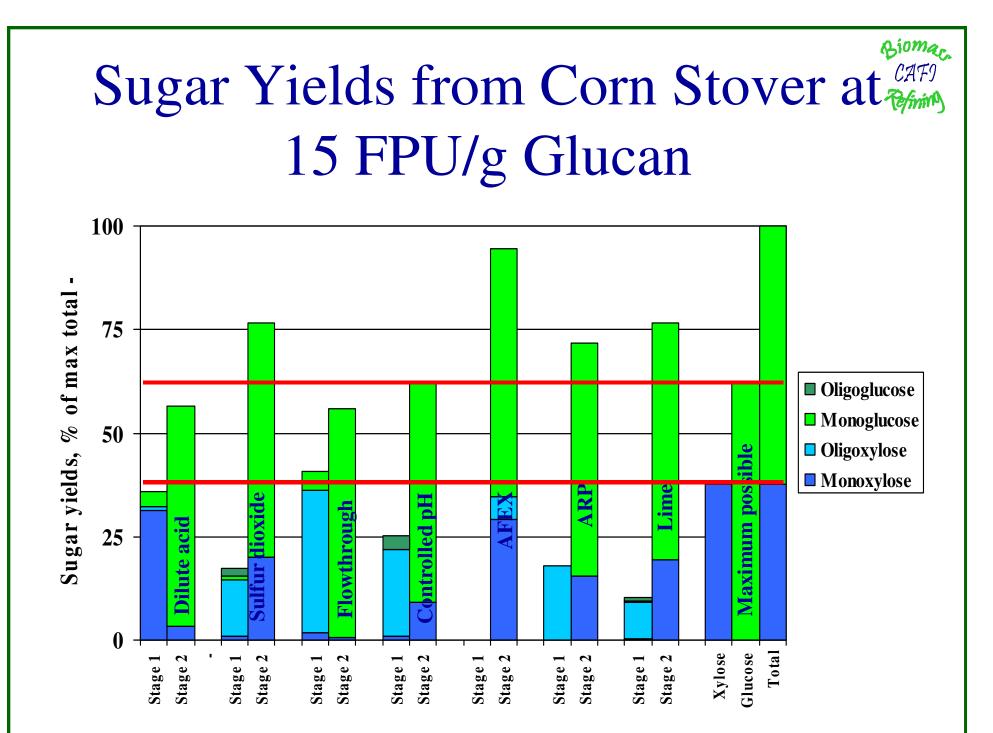


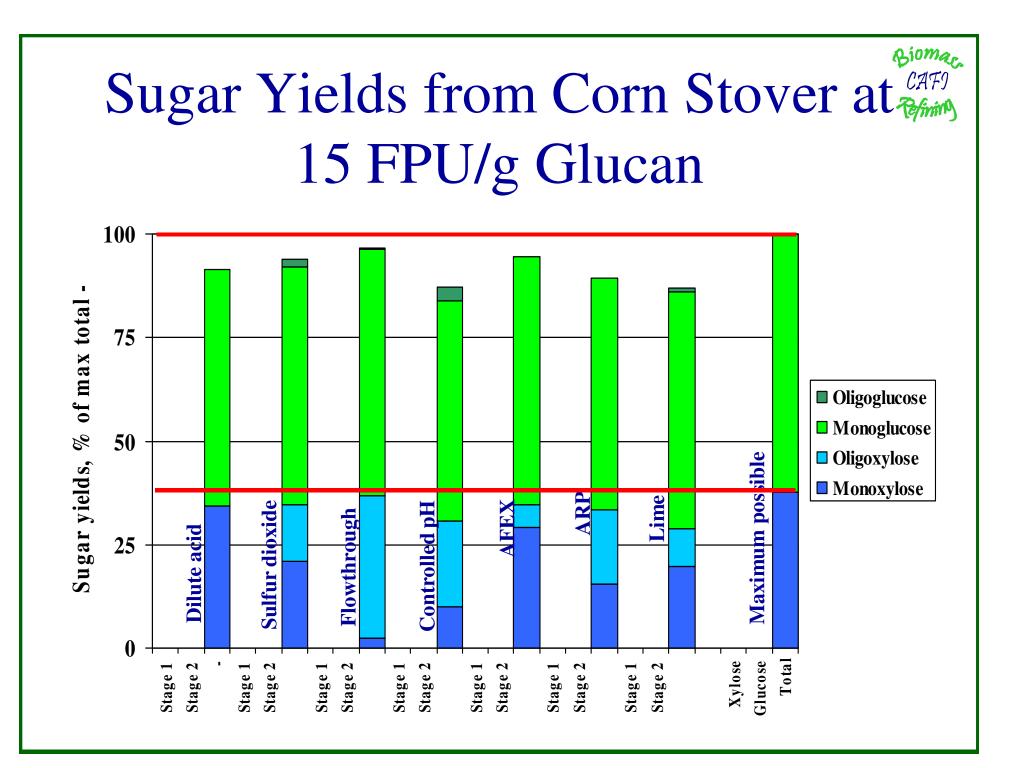




Sugar Yields from Corn Stover at CATO 15 FPU/g Glucan







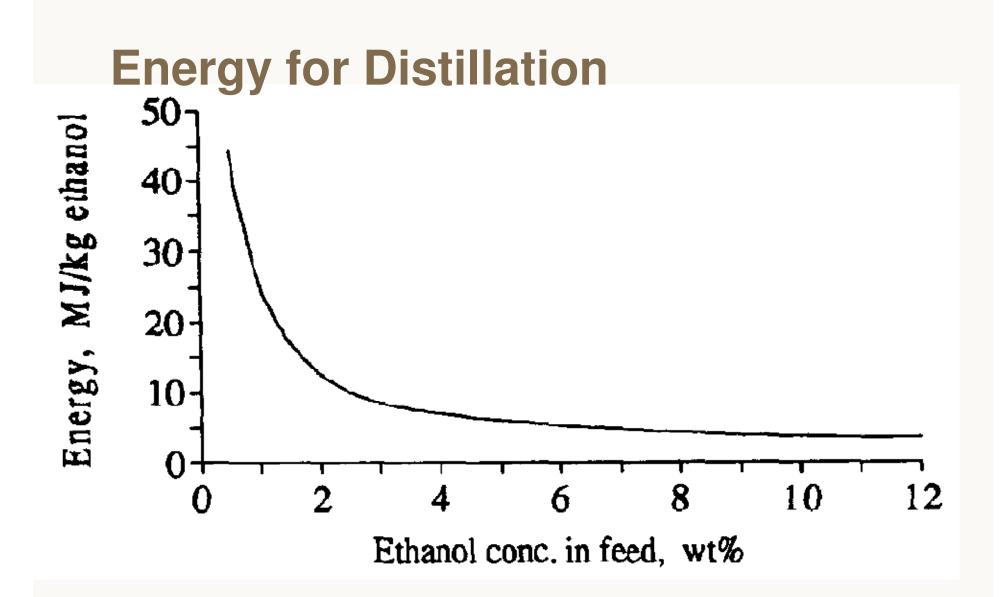
Process Considerations

- 1. Process Integration how pretreatment streams integrated into production process
- Yield (outlined above) -> gallons of ethanol per ton biomass
- 3. Energy -> \$ per gallon of ethanol

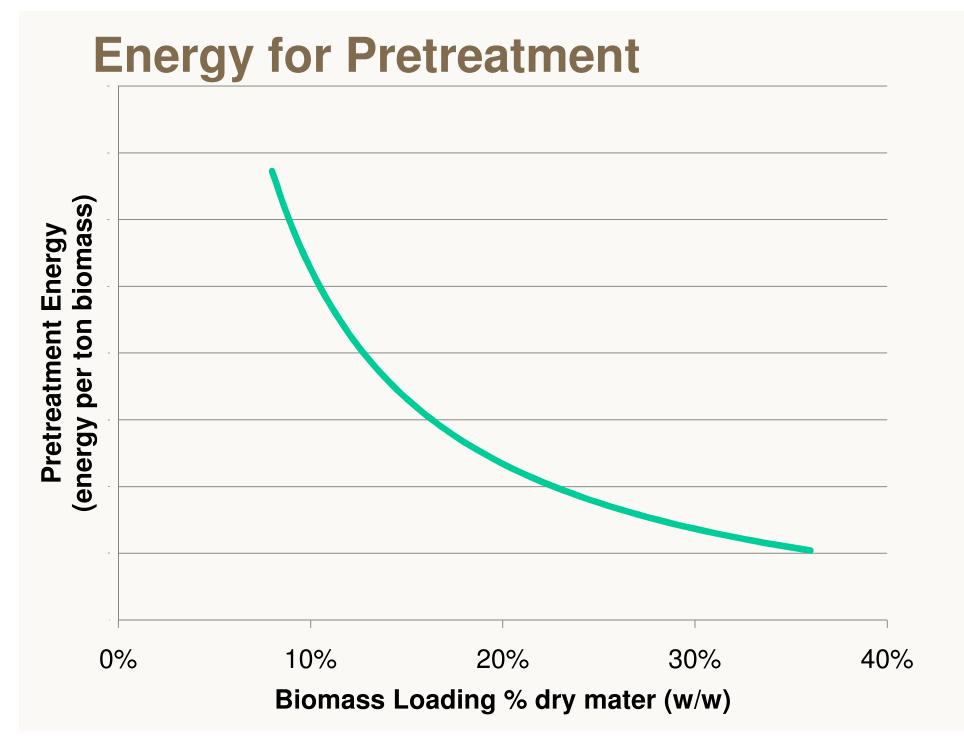
Higher yield is better

Lower cost is better





Galbe, M., Sassner, P., Wingren, A., Zacchi, G. (2007). Process engineering economics of bioethanol production. <u>Biofuels</u>. Berlin, Springer-Verlag Berlin. **108**: 303-327.



Practical Fuel Ethanol Production

>At least 6% (w/v) ethanol

- >Means: 13% (w/v) sugars (90% yield)
- Requires: 30 40% (w/v) feedstock in water



Pretreated DG – Effect of Solids Loading



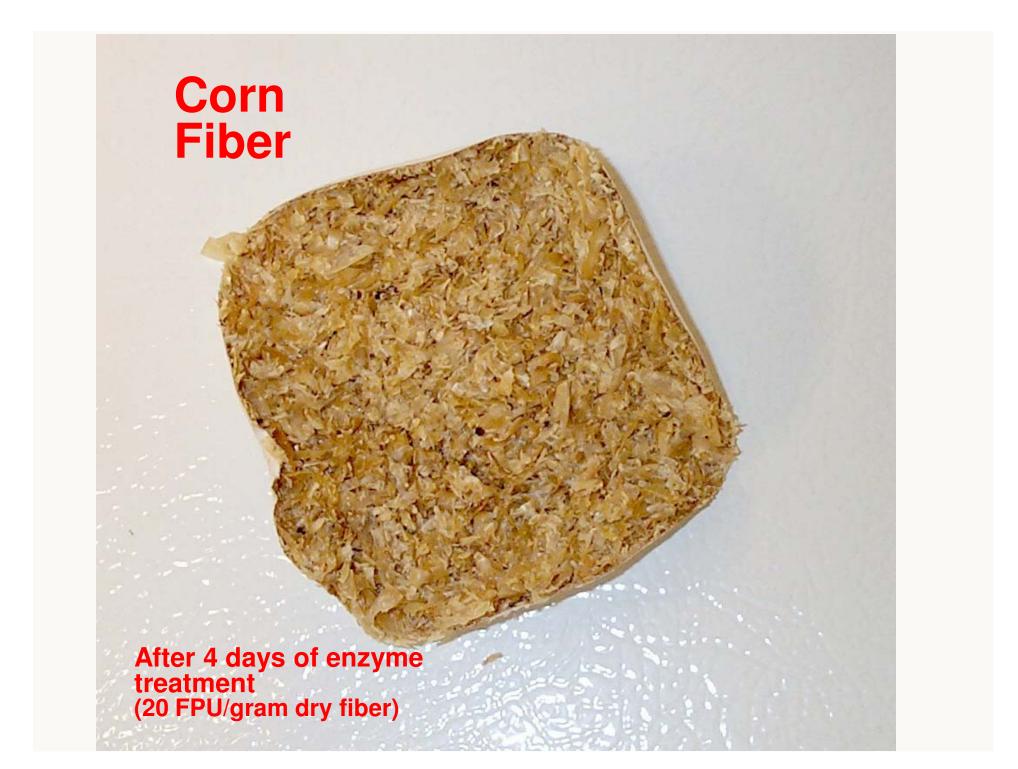


Pretreated DG – Effect of Enzymatic Hydrolysis (1.5 hrs)

Liquefaction by enzyme hydrolysis



No additional liquid added



Pretreated Corn Fiber 160°C, 20 min.

After 1 day of enzyme treatment (20 FPU/gram dry fiber)

Sugar Yields: 24 hr Hydrolysis with Cellulase

24 Hours of Hydrolysis by 15 FPU/g glucan in DG Cellulase + 40 IU/g glucan β -glucosidase

Sugar (g/L)	15%	20%	30%
	Solids	Solids	Solids
Glucose (g/L)	26.0	32.8	42.2
(% yield)	68%	71%	73%
Xylose (g/L)	4.5	5.8	2.8
(% yield)	19%	19%	19%

% yield includes polysaccharides from both DG and stillage

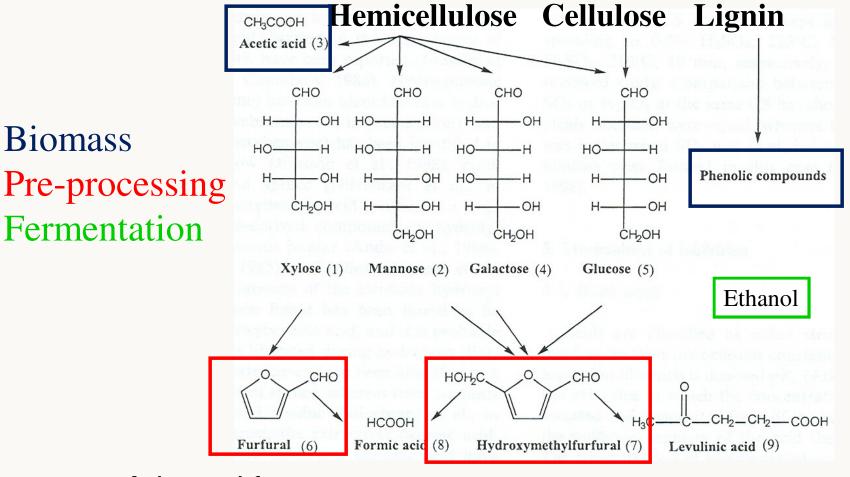


Viscosity

- Must be able to move (pump) slurry between unit operations
- Must be able to effectively mix slurry during processing (especially hydrolysis and fermentation)
- Energy for pumping and mixing should be minimized



Sources of Inhibitors to Biocatalyts



Adapted from Palmqvist *et al.* <u>Bioresource Technology</u> 74:25-33 (2000)

Wet (ensiled) storage

- Low pH for long term storage
- Reduced dry matter losses
- Platform for biological pretreatment
- But increased organic acids...

















Pretreatment Needs

- > Liquid hot water-like technology
- > Limited chemical use
- Reduced milling: Use chips not sawdust
- > Low cost materials of construction
- > High hemicellulose yields
- > High yields of glucose from cellulose
- Robust performance with multiple feedstocks



Conclusions

- Pretreatment keystone technology for biological route to biofuels
- Pretreatment enhances rate and yield of sugar release from lignocellulosic biomass
- Pretreatment is thermochemical process that fractionates and/or alters physiochemical structure of biomass
- Pretreatment technologies employ wide array of solvents/catalysts
- Process integration key to evaluating pretreatment technology for commercial application



